Wednesday, 20 May 2020 2016 Q3 (b) no flux r=1, u=0 on no slip on a r=lj V = 1 on moving boundary on the solid object on the free  $\frac{\partial}{\partial t} \left( r - h(0, k) \right) = 0$   $\Rightarrow u = \frac{\partial}{\partial t} + v \frac{\partial}{\partial 0}$ surface at r-h(0,E)=0Dynamic conditions on the free surface: Jon=0 as there's a vacuum outside, so == o outside, and J'n 3 continuous at the fire surface. ひってい コロ ラヤコの  $\underline{t} \cdot \underline{c} \cdot \underline{n} = 0$ In (r,0) coordinates  $\Xi = \begin{pmatrix} -P + 2\mu \frac{3\mu}{3r} & \mu(\frac{3\nu}{3r} + \frac{3\mu}{30}) \\ \mu(\frac{3\nu}{3r} + \frac{3\mu}{30}) & -P + 2\mu \frac{3\nu}{30} \end{pmatrix}$ in the thin fiten approximation with dimensionless vadires!

Wednesday, 27 May 2020 2016 92 (a) Put  $v = S_z V(x, Y)$ ,  $y = S_i Y$ 0 = 7.4 = 34 + 34  $= \frac{\partial u}{\partial z} + \frac{S_2}{S_1} \frac{\partial v}{\partial \gamma}$ Go choose  $\partial_1 = \partial_2$ .  $U \frac{\partial u}{\partial x} + V \frac{\partial u}{\partial y} = -\frac{\partial P}{\partial x} + \frac{1}{Pe} \left( \frac{\partial^2 u}{\partial x^2} + \frac{1}{S_1^2} \frac{\partial^2 u}{\partial y^2} \right)$ Choose Si= Re 1/2 to get  $U \frac{\partial u}{\partial x} + V \frac{\partial u}{\partial y} = -\frac{\partial P}{\partial x} + \frac{\partial^2 u}{\partial y^2} + \frac{1}{Re} \frac{\partial^2 u}{\partial x^2}$ Expanding u=u0+ Re-1/2 U1+-yours Uo 3th + Vo 37 = - 3x + 3200 Uo 3x + Vo 37 = - 3x + 372 at leading order.

Wednesday, 27 May 2020 2016 Q1(b) We're bld u = u(x,y,z,t)iP(3t +4. Va) = - Vp + vp \ 24 V.u = 0  $\nabla p = -p G \cos(\omega E) \frac{i}{2} 50$  $\frac{\partial \mathcal{L}}{\partial t} + \mathcal{L} \cdot \mathcal{V} \mathcal{L} = - G \cos(\omega t) \hat{\mathcal{L}}$ to Pau  $0 = V_{ou} = \frac{\partial u}{\partial x}$ so U= U(Y,Z,E) = > 4. Pu = 0 Gcos (wt) = + 0 P'u in the half-space y>0. The domain is independent of Z, so we can take u to be independent of Z, and find a solution for U(5,t). This is consistent with P. u=0 go ne dou't need an æddetrænel pressure grædtent. 2016 Q1. 20th May 2020 morning session!  $u(y,t) = sint + e^{-\frac{y}{5\pi}} sin \left(\frac{y}{5\pi} - t\right)$ The sbess on the plate  $3\frac{3u}{3y}|_{y=0}$ .

dimensionless  $\frac{3u}{3y} = e^{-\sqrt{3u}} \left(-\sin\left(\frac{y}{\sqrt{2u}} - t\right) + \cos\left(\frac{y}{\sqrt{2u}} - t\right)\right)$  $= (\operatorname{sunt} + \operatorname{cost}) \frac{1}{\sqrt{2}}$   $= \operatorname{sun} (t + T/4)$ = JT (sunt cos TT + costsuh (T) as sun T/4 = cos T/4 = 521 un sunt as y->0 is The out of phase un (y, t).  $\frac{\partial u}{\partial t} = G\cos(\omega t) + v \frac{\partial^2 u}{\partial y^2}$ The plate at y=0 is stationary, y=0 so u=0 on y=0. For from the plate (y>>1) ne expect u to be independent of y, learny  $\frac{\partial u}{\partial t} = G\cos(\omega t)$   $u \sim G\sin(\omega t).$ 

Notes, page 20

Notes, page 20

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 $\frac{1}{2}(n \cdot r) = -$ 

Example 2-6.4 in the notes (p.43) Prandtl's idea 3 that the flow comprises on chriscol -> outer flow and a thing Vizcous boundary Layer. For inviscial flow around a cylinder: The incoming uniform stream has no vortraits, and inviscial flows can't create vortraits, so We need  $P \cdot u = P^2 / = 0$ , and  $u_r = \frac{\partial u}{\partial r} = 0$  on r = 1 (cylinder) Uz = Urcoso - Uosino -> / as r-> co let's by  $\emptyset = f(r) \cos \theta$ .  $U_r = \mathcal{Z} = f'(r) \cos \vartheta$  $u_0 = \frac{1}{7} \frac{3\phi}{30} = -\frac{f(r)}{r} sin 0$ The solutions of Laplace's equation of the form  $\beta = f(r)\cos\theta$  are rcoso or tcoso. Imposing  $\frac{\partial \mathcal{L}}{\partial r} = 0$  on r = 1 and proso = x as r 70 determines  $\phi = (r + \frac{1}{r})\cos \theta$ . Now re how the outer flow and hence Us, but we need to put it into boundary layer coordinates.

TY coordinates.

Onginally ne had We can wap this around a cured serface provided the radius of curative is much bigger than the boundary loyer thickness. or is measured tongentially (are longth) along the boundary from the front, the forward stagnation point. I is measured normally from the boundary. In the BL,  $u(x, Y) \rightarrow U_s(x)$ as Y->00, where  $U_5(x) = \frac{um}{y \Rightarrow 0} \text{ Monter}(x,y).$ In other words, um  $U_{BL}(x,y) = um$   $U_{outer(x,y)}$   $y \to \infty$   $U_{BL}(x,y) = y \to \infty$  $= U_s(x).$ The for field flow books like: Slow speeds This is the for field relative to the thin boundary layer, but not relative to the cylinder. x= T-0 on r=1 The tengential velocity in the uniqued outer flow as ne approach the cylinder  $\frac{UM - UO(x,y)}{y - 30} = -\frac{30}{30} (r = 1,0 = 11-2)$  $= (1+1)(-sin(\pi-x))$ = 29ch x  $= U_5(x)$ x=11/2, Us=Z Bernoulli relates po(x) to Os (x) on the chiraced flow: po (x) + = Us (x) is constant. Differentiating w.r.t. & givs  $\frac{dpo}{dx} = -Us \frac{dUs}{dsc} = -Zsuhx (Zcosx)$ =-Zsch(2x) $P_0(x) = \cos(2x) - 1$ with the constant chosen to make po=0, at x=0, TT, the stægnation pourts. 1 foravable mt/2 unfavourable In the Falhner-Shar model with Us(x) is accelerating with increasing x (i.e. favourable pressue gradient) for m>0, and decelerating with hoverschg a for m<0. Solutions to the Falhner-Shar equetions exist for m>-0.0904 à little way unto m<0.